Heat Transfer Problems

Introductory Course on Multiphysics Modelling

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Outline

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Three mechanisms of heat transfer

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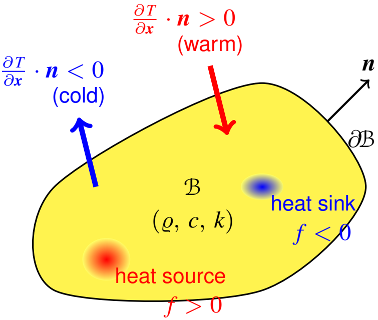
Motivation for dealing with heat transfer problems:

- In many engineering systems and devices there is often a need for **optimal thermal performance**.
- Most **material properties are temperature-dependent** so the effects of heat transfer enter many other disciplines and drive the requirement for **multiphysics modeling**.

Heat conduction and the energy conservation law



- *Problem*: to find the **temperature** in a solid, $T = T(\boldsymbol{x}, t) = ?\ [\mathrm{K}]$.
- **Temperature** is related to **heat** which is a form of **energy**.
- The **principle of conservation of energy** should be used to determine the temperature.
- Thermal energy can be: **stored**, **generated** (or absorbed), and **supplied** (transferred).

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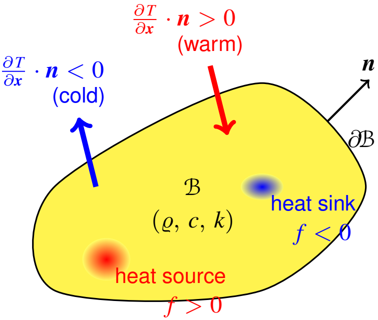

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The law of conservation of thermal energy

The rate of change of internal thermal energy with respect to time in $\mathcal{B}$ is equal to the net flow of energy across the surface of $\mathcal{B}$ plus the rate at which the heat is generated within $\mathcal{B}$.

Outline

Balance of thermal energy

- The internal **thermal energy**, E $[\mathrm{J}]$:

$$\int_{\mathcal{B}} \varrho \, e \, \mathrm{d}V$$

$\varrho = \varrho(\boldsymbol{x})$ – the mass density $\left[\frac{\mathrm{kg}}{\mathrm{m}^3}\right]$

$e = e(\boldsymbol{x}, t)$ – the specific internal energy $\left[\frac{\mathrm{J}}{\mathrm{kg}}\right]$

Balance of thermal energy

- The **rate of change of thermal energy**, $\dot{E} = \frac{\mathrm{d}E}{\mathrm{d}t}$ $[\mathrm{W}]$:

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- The **flow of heat**, Q $[\mathrm{W}]$ (the amount of heat per unit time flowing-in across the boundary $\partial\mathcal{B}$):

$$-\int_{\partial\mathcal{B}} \boldsymbol{q} \cdot \boldsymbol{n} \, \mathrm{d}S$$

$\boldsymbol{q} = \boldsymbol{q}(\boldsymbol{x}, t)$ – the heat flux vector $\left[\frac{\mathrm{W}}{\mathrm{m}^2}\right]$

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- The total **rate of heat production**, F $[\mathrm{W}]$ (the amount of heat per unit time produced in $\mathcal{B}$ by the volumetric heat sources):

$$\int\limits_{\mathcal{B}} f \,\mathrm{d}V$$

$f = f(\boldsymbol{x}, t)$ – the rate of heat production per unit volume $\left[\frac{\mathrm{W}}{\mathrm{m}^3}\right]$

Balance of thermal energy

The thermal energy conservation law, $\dot{E} = Q + F$, leads to the following balance equation.

The global form of thermal energy balance

$$\int\limits_{\mathcal{B}} \varrho \frac{\partial e}{\partial t} \, \mathrm{d}V = - \int\limits_{\partial\mathcal{B}} \boldsymbol{q} \cdot \boldsymbol{n} \, \mathrm{d}S + \int\limits_{\mathcal{B}} f \, \mathrm{d}V$$

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$$\int_{\mathcal{B}} \varrho \frac{\partial e}{\partial t} \, \mathrm{d}V = - \int_{\mathcal{B}} \nabla \cdot \boldsymbol{q} \, \mathrm{d}V + \int_{\mathcal{B}} f \, \mathrm{d}V$$

(after using the divergence theorem)

Balance of thermal energy

The thermal energy conservation law, $\dot{E} = Q + F$, leads to the following balance equation.

The global form of thermal energy balance

$$\int_{\mathcal{B}} \left(\varrho \, \frac{\partial e}{\partial t} + \nabla \cdot \boldsymbol{q} - f \right) \mathrm{d}V = 0 \,.$$

Assuming the continuity of the above integral and using the fact that this equality holds not only for the whole domain $\mathcal{B}$, but also for its every single subdomain the following PDE is obtained.

The local form of thermal energy balance

$$\varrho \, \frac{\partial e}{\partial t} + \nabla \cdot \boldsymbol{q} = f \quad \text{in } \mathcal{B} \,.$$

- The unknown fields are: $e = e(\boldsymbol{x}, t) = ?$, $\boldsymbol{q} = \boldsymbol{q}(\boldsymbol{x}, t) = ?$.
- The fields are related to the unknown temperature $T = T(\boldsymbol{x}, t) = ?$.
- The relations $e = e(T)$ and $\boldsymbol{q} = \boldsymbol{q}(T)$ are to be established and applied.

Specific thermal energy: a constitutive relation

Observation:

- For many materials, over fairly wide (but not too large) temperature ranges, the specific thermal energy depends **linearly** on the temperature.

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Specific thermal energy vs. temperature

$$\frac{\partial e}{\partial t} = c\,\frac{\partial T}{\partial t}$$

where $c = c(\boldsymbol{x}, t)$ is the **thermal capacity** $\left[\frac{\mathrm{J}}{\mathrm{kg}\cdot\mathrm{K}}\right]$.

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- The thermal capacity is also called the *specific heat capacity* (at a constant pressure), or simply, the *specific heat*).
- It describes the ability of a material to store the heat and refers to the quantity that represents the amount of heat required to change the temperature of one unit of mass by one degree.

(Isobaric mass) thermal capacity

Material	c $\left[\frac{\mathrm{J}}{\mathrm{kg \cdot K}}\right]$
Aluminium	897
Steel	466
Glass	84
Water (solid: ice at -10°C)	2 110
Water (liquid at 25°C)	4 181
Water (gas: steam at 100°C)	2 080
Air (at room conditions)	1 012

Fourier's law of heat conduction

Observations:

- the **heat flows** from regions of **high temperature to** regions of **low temperature**,
- the rate of heat **flow is bigger** if the **temperature differences** (between neighboring regions) are **larger**.

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Postulate: there is a **linear relationship** between the rate of **heat flow** and the rate of **temperature change**.

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$$\boldsymbol{q} = -k \, \nabla T$$

where $k = k(\boldsymbol{x})$ is the **thermal conductivity** $\left[\frac{\mathrm{W}}{\mathrm{m \cdot K}}\right]$.

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- The **thermal conductivity** is a material constant that describes the ability of a material to conduct the heat.
- If the thermal conductivity is anisotropic, k becomes a (second order) *thermal conductivity tensor*.

Thermal conductivity

Material	$k\ \left[\frac{\mathrm{W}}{\mathrm{m \cdot K}}\right]$
Aluminium	220
Steel (carbon)	50
Steel (stainless)	18
Glass	1.0
Water (liquid)	0.6
Air (gas)	0.025

Derivation of the heat equation

Energy vs. temp.

$$\frac{\partial e}{\partial t} = c\,\frac{\partial T}{\partial t}$$

Energy conservation law

$$\varrho\,\frac{\partial e}{\partial t} + \nabla \cdot \boldsymbol{q} = f$$

Fourier's law

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Fourier's law

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Heat conduction equation

$$\varrho\,c\,\frac{\partial T}{\partial t} - \nabla \cdot (k\,\nabla T) = f$$

where the only unknown is the temperature: $T(\boldsymbol{x}, t) = ?$

Derivation of the heat equation

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Thermally-homogeneous material: For $k(\boldsymbol{x}) =$ const. the heat PDE can be presented as follows

$$\frac{\partial T}{\partial t} = \alpha^2\,\triangle T + \tilde{f} \quad \text{where} \quad \alpha^2 = \frac{k}{\varrho\,c} \quad \text{and} \quad \tilde{f} = \frac{f}{\varrho\,c}\,.$$

Here: $\alpha^2 = \alpha^2(\boldsymbol{x})$ is the thermal diffusivity $\left[\frac{\mathrm{m}^2}{\mathrm{s}}\right]$,
$\tilde{f} = \tilde{f}(\boldsymbol{x},t)$ is the rate of change of temperature $\left[\frac{\mathrm{K}}{\mathrm{s}}\right]$ due to internal heat sources.

Outline

Boundary conditions

The mathematical point of view

From the point of view of mathematics there are **three kinds** of boundary conditions:

1. the **first kind** or **Dirichlet** b.c. – to set a *temperature*, $\hat{T}$ $[\mathrm{K}]$, on a boundary:

$$T = \hat{T} \quad \text{on } \partial\mathcal{B}_T,$$

Here, $\partial\mathcal{B}_T$, $\partial\mathcal{B}_q$, and $\partial\mathcal{B}_h$ are mutually disjoint, complementary parts of the boundary $\partial\mathcal{B}$.

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2. the **second kind** or **Neumann** b.c. – to set an *inward heat flux*, $\hat{q}$ $[\mathrm{W}]$, normal to the boundary:

$$-\boldsymbol{q}(T) \cdot \boldsymbol{n} = \hat{q} \quad \text{on } \partial\mathcal{B}_q,$$

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3. the **third kind** or **Robin** (or **generalized Neumann**) b.c. – to specify the heat flux in terms of an explicit *heat flux*, $\hat{q}$, and a *convective heat transfer coefficient*, h $\left[\frac{\mathrm{W}}{\mathrm{m}^2 \cdot \mathrm{K}}\right]$, relative to a *reference temperature*, $\hat{T}$:
$$-\boldsymbol{q}(T) \cdot \boldsymbol{n} = \hat{q} + h\left(\hat{T} - T\right) \quad \text{on } \partial\mathcal{B}_h.$$

Here, $\partial\mathcal{B}_T$, $\partial\mathcal{B}_q$, and $\partial\mathcal{B}_h$ are mutually disjoint, complementary parts of the boundary $\partial\mathcal{B}$.

Boundary conditions

The physical interpretations

Prescribed temperature : $T = \hat{T}$

Along a boundary the specified temperature, $\hat{T}$, is maintained (the surrounding medium is thermostatic).

*Use the **Dirichlet** b.c. Specify:* $\hat{T}$.

Boundary conditions

The physical interpretations

Prescribed temperature : $T = \hat{T}$

Use the ***Dirichlet*** *b.c. Specify:* $\hat{T}$*.*

Insulation or symmetry : $-\boldsymbol{q}(T) \cdot \boldsymbol{n} = 0$

To specify where a domain is well insulated, or to reduce model size by taking advantage of symmetry. The condition means that the temperature gradient across the boundary must equal zero. For this to be true, the temperature on one side of the boundary must equal the temperature on the other side (heat cannot transfer across the boundary if there is no temperature difference).

Use the (homogeneous) ***Neumann*** *b.c. with* $\hat{q} = 0$*.*

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Conductive heat flux : $-\boldsymbol{q}(T) \cdot \boldsymbol{n} = \hat{q}$

To specify a heat flux, $\hat{q}$, that enters a domain. This condition is well suited to represent, for example, any electric heater (neglecting its geometry).

*Use the **Neumann** b.c. Specify: $\hat{q}$.*

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*Use the **Neumann** b.c. Specify: $\hat{q}$.*

Convective heat flux : $-\boldsymbol{q}(T) \cdot \boldsymbol{n} = h\,(\hat{T} - T)$

To model convective heat transfer with the surrounding environment, where the heat transfer coefficient, h, depends on the geometry and the ambient flow conditions; $\hat{T}$ is the external bulk temperature.

*Use the **Robin** b.c. with $\hat{q} = 0$. Specify: h and $\hat{T}$.*

Boundary conditions

The physical interpretations

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*Use the **Robin** b.c. with* $\hat{q} = 0$. *Specify:* h *and* $\hat{T}$.

Heat flux from convection and conduction : $-\boldsymbol{q}(T) \cdot \boldsymbol{n} = \hat{q} + h\,(\hat{T} - T)$

Heat is transferred by convection and conduction. Both contributions are significant and none of them can be neglected. Notice that the conduction heat flux, $\hat{q}$, is in the direction of the inward normal whereas the convection term, $h\,(\hat{T} - T)$, in the direction of the outward normal.

*Use the **Robin** b.c. Specify:* h, $\hat{T}$, *and* $\hat{q}$.

Initial-Boundary-Value Problem

IBVP of the heat transfer

Find $T = T(\boldsymbol{x}, t)$ for $\boldsymbol{x} \in \mathcal{B}$ and $t \in [t_0, t_1]$ satisfying the **heat equation**:

$$\varrho\, c\, \dot{T} + \nabla \cdot \boldsymbol{q} - f = 0 \quad \text{where} \quad \boldsymbol{q} = \boldsymbol{q}(T) = -k\, \nabla T\,,$$

with the **initial condition** (at $t = t_0$):

$$T(\boldsymbol{x}, t_0) = T_0(\boldsymbol{x}) \quad \text{in } \mathcal{B}\,,$$

and subject to the **boundary conditions**:

$$T(\boldsymbol{x}, t) = \hat{T}(\boldsymbol{x}, t) \;\text{ on } \partial\mathcal{B}_T\,,$$

$$-\boldsymbol{q}(T)\,\boldsymbol{n} = \hat{q}(\boldsymbol{x}, t) \;\text{ on } \partial\mathcal{B}_q\,,$$

$$-\boldsymbol{q}(T) \cdot \boldsymbol{n} = \hat{q} + h\,(\hat{T} - T) \;\text{ on } \partial\mathcal{B}_h\,,$$

where $\partial\mathcal{B}_T \cup \partial\mathcal{B}_q \cup \partial\mathcal{B}_h = \partial\mathcal{B}$, and the parts of boundary $\partial\mathcal{B}$ are mutually disjoint: $\partial\mathcal{B}_T \cap \partial\mathcal{B}_q = \emptyset$, $\partial\mathcal{B}_T \cap \partial\mathcal{B}_h = \emptyset$, $\partial\mathcal{B}_q \cap \partial\mathcal{B}_h = \emptyset$.

Outline

Heat transfer by convection (and conduction)

An important mechanism of heat transfer in fluids is **convection**.

- Heat can be transferred with fluid in motion.
- In such case, a **convective term** containing the convective velocity vector, $\boldsymbol{u}\ \left[\frac{\mathrm{m}}{\mathrm{s}}\right]$, must be added to the Fourier's law of heat conduction:

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(Conservative) heat transfer equation with convection

$$c\,\frac{\partial(\varrho\, T)}{\partial t} + \nabla\cdot\left(-k\,\nabla T + \varrho\, c\, \boldsymbol{u}\, T\right) = f\,.$$

Notice that here the density is allowed to be time-dependent, $\varrho = \varrho(\boldsymbol{x}, t)$, since it can change in time and space due to the fluid motion causing local compressions and decompressions.

Non-conservative convective heat transfer

For homogeneous, **incompressible** fluid:

$$\nabla \cdot \boldsymbol{u} = 0 \quad \rightarrow \quad \varrho(\boldsymbol{x}, t) = \mathrm{const}\,.$$

This assumption produces the following result

$$\nabla \cdot (\varrho\, c\, \boldsymbol{u}\, T) = \varrho\, c\, \nabla T \cdot \boldsymbol{u} + \underbrace{T\, \nabla \cdot (\varrho\, c\, \boldsymbol{u})}_{0} = \varrho\, c\, \nabla T \cdot \boldsymbol{u}\,.$$

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Non-conservative heat transfer equation with convection

$$\varrho\, c\, \frac{\partial T}{\partial t} - \nabla \cdot (k\, \nabla T) + \varrho\, c\, \nabla T \cdot \boldsymbol{u} = f\,,$$

or, for $k(\boldsymbol{x}) = \text{const}\,.$: $\quad \dfrac{\partial T}{\partial t} = \tilde{f} + \alpha^2\, \triangle T - \nabla T \cdot \boldsymbol{u}\,.$